

[Contribution from the Department of Chemistry,  
Massachusetts Institute of Technology]

Displacement Reactions. XII.<sup>1</sup> Correlation of Rates of Solvolysis  
with a Four-Parameter Equation

(1) Paper XI<sup>2</sup> serves as an introduction to this paper. This work was supported by the Office of Naval Research.

(2) C. G. Swain, R. E. Mosely, D. E. Bown, I. Allen and D. C. Dittmer, J. Am. Chem. Soc., 76, 000 (1954).

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A four-parameter equation,  $\log (k/k^{\circ}) = c_1 d_1 + c_2 d_2$ , is tested, where  $k$  is the first-order rate constant for solvolysis of any compound in any medium,  $k^{\circ}$  is the corresponding rate constant in a standard medium (80% ethanol) at the same temperature,  $c_1$  and  $c_2$  are constants depending only on the compound undergoing solvolysis, and  $d_1$  and  $d_2$  are constants depending only on the medium. All available data capable of serving as a test of the equation were used. Values of  $c_1$  and  $c_2$  are reported for 25 compounds ranging from p-nitrobenzoyl chloride to triphenylmethyl fluoride, and values of  $d_1$  and  $d_2$  for 18 solvents ranging from methanol to formic acid. These were determined from the equation and 146 observed  $\log (k/k^{\circ})$  values by the method of least squares. The mean and maximum ranges in observed rate for a fixed compound are factors of  $1.4 \times 10^3$  and  $7.6 \times 10^6$  respectively. The mean and maximum errors in the calculated rate are factors of 1.33 and 4.4.

A four-parameter equation was developed in paper XI<sup>2</sup>

$$\log (k/k^{\circ}) = c_1 d_1 + c_2 d_2$$

where  $k$  is the first-order rate constant for solvolysis of any compound in any medium,  $k^{\circ}$  is the corresponding rate constant in a standard medium at the same temperature,  $c_1$  and  $c_2$  are constants depending only on the

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compound undergoing solvolysis, and  $\underline{d}_1$  and  $\underline{d}_2$  are constants depending only on the solvent.

As the standard solvent we chose 80% ethanol-20% water by volume because more data were available for it than for any other solvent. Table I lists  $\log k_o$  in 80% ethanol for 25 compounds.

Table II lists the  $146 \log (k/k^\circ)$  values capable of serving as a check on the equation,<sup>3</sup> i.e., for solvents studied with three or more compounds

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(3) The only data knowingly omitted were 6 data on *t*-butyl bromide, which were used in preliminary attempts to fit the equation but were dropped in the course of the Mark IV calculation because they appeared to interfere with convergence of the successive approximation procedure employed.

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or for compounds studied in four or more solvents at the same temperature, or at enough temperatures to permit extrapolation to the common temperature for each compound listed in Table I.

Table I

RATES IN 80% ETHANOL

Compound <sup>a</sup>	$\log_{10} k^\circ, \text{sec.}^{-1}$	Temp., °C.	Ref.
$\text{NO}_2\phi\text{COCl}$	-1.31	25	4
$\text{NO}_2\phi\text{COF}$	-2.00	25	4
$\phi\text{COCl}$	-2.59	25	4
$\phi\text{COF}$	-4.21	25	4
$\text{Me}\phi\text{COCl}$	-2.46	25	4
$\text{Me}\phi\text{COF}$	-4.67	25	4
$\text{MeBr}$	-5.66	50	5,6
$\text{EtBr}$	-5.86	50	5,6
$\text{EtOTs}$	-5.04	50	5
$n\text{-BuBr}$	-5.41 <sup>b</sup>	75.1	7
$\phi\text{CH}_2\text{Cl}$	-5.65	50	5
$\phi\text{CH}_2\text{OTs}$	-3.49	25	5
$i\text{-PrBr}$	-5.93	50	5
$i\text{-PrOBs}$	-2.77	70	8
$\text{PinCBs}$	-2.86	70	8
$\text{MeOCxOBs}$	-5.49	50	5
$\text{BrCxOBs}$	-5.15	50	5
$\phi\text{CHClMe}$	-3.79	50	9
$\phi_2\text{CHCl}$	-2.77	25	10
$\phi_2\text{CHF}$	-6.56	25	11
$t\text{-BuCl}$	-5.03	25	12
$\phi_3\text{CSCN}$	-2.98 <sup>c</sup>	25	11
$\phi_3\text{COAc}$	-3.28	25	11
$\phi_3\text{CO}\phi\text{NO}_2$	-3.35	25	11
$\phi_3\text{CF}$	-3.58	25	11

<sup>a</sup>  $\phi = \text{C}_6\text{H}_5$  or *p*-substituted  $\text{C}_6\text{H}_4$ ;  $\text{BrCx}$  = *trans*-2-bromocyclohexyl;  $\text{Pin}$  = pinacolyl;  $\text{OTs}$  = *p*-toluenesulfonate;  $\text{CBs}$  = *p*-bromobenzenesulfonate;  $\text{Me}$ ,  $\text{Et}$ ,  $\text{Pr}$ ,  $\text{Bu}$  =  $\text{CH}_3$ ,  $\text{C}_2\text{H}_5$ ,  $\text{C}_3\text{H}_7$ ,  $\text{C}_4\text{H}_9$ .

<sup>b</sup> Interpolated from a plot of  $\log k$  vs. mole fraction of water.

<sup>c</sup> Assumed value. No measurements were made in 80% ethanol.

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Table II

RELATIVE RATES OF SOLVOLYSIS<sup>a</sup>

Compound <sup>b</sup>	Solvent <sup>c</sup>	$\log (k/k^{\circ})^a$	Ref.
NO <sub>2</sub> φCOCl	EtOH, 100	-0.68	4
"	Me <sub>2</sub> CO, 90	- .91	4
"	Me <sub>2</sub> CO, 80	- .52	4
"	Me <sub>2</sub> CO, 70	- .35	4
"	Me <sub>2</sub> CO, 50	- .12	4
"	AcOH, 100	-4.67	4
"	HCOOH, 100	-3.37	4
NO <sub>2</sub> φCOF	MeOH, 100	-1.59	4
"	MeOH, 96.7	-0.51	4
"	MeOH, 69.5	+ .47	4
"	EtOH, 100	-1.77	4
"	EtOH, 40	+0.51	4
"	Me <sub>2</sub> CO, 80	-1.07	4
"	Me <sub>2</sub> CO, 70	-0.64	4
"	Me <sub>2</sub> CO, 50	-0.04	4
"	AcOH, 100 <sup>d</sup>	-6.37	4
"	HCOOH, 100	-4.25	4
φCOCl	MeOH, 100	+0.22	13
"	MeOH, 96.7	+ .33	4
"	MeOH, 69.5	+ .87	4
"	EtOH, 100	- .52	4
"	EtOH, 60	+ .48	4
"	EtOH, 50	+ .84	4
"	EtOH, 40	+1.30	4
"	Me <sub>2</sub> CO, 90	-1.18	4
"	Me <sub>2</sub> CO, 80	-0.72	4

(Table II continued)

Compound	Solvent	$\log (k/k^0)$	Ref.
$\phi\text{COCl}$	$\text{Me}_2\text{CO}$ , 70	-0.37	4
"	$\text{Me}_2\text{CO}$ , 50	+ .50	4
"	$\text{AcOH}$ , 100	-2.39	4
$\phi\text{COF}$	$\text{MeOH}$ , 96.7	-0.23	4
"	$\text{MeOH}$ , 69.5	+ .84	4
"	$\text{EtOH}$ , 100	-1.53	4
"	$\text{EtOH}$ , 40	+0.81	4
"	$\text{Me}_2\text{CO}$ , 80	-1.19	4
"	$\text{Me}_2\text{CO}$ , 70	-0.67	4
"	$\text{Me}_2\text{CO}$ , 50	+ .11	4
"	$\text{AcOH}$ , 100 <sup>d</sup>	-4.47	4
"	$\text{HCOOH}$ , 100	-1.61	4
$\text{Me}\phi\text{COCl}$	$\text{EtOH}$ , 100	-0.79	13
"	$\text{Me}_2\text{CO}$ , 80	- .90	4
"	$\text{Me}_2\text{CO}$ , 50	+ .85	4
"	$\text{AcOH}$ , 100	-1.94	4
$\text{Me}\phi\text{COF}$	$\text{Me}_2\text{CO}$ , 80	-1.13	4
"	$\text{Me}_2\text{CO}$ , 50	+0.09	4
"	$\text{AcOH}$ , 100 <sup>d</sup>	-3.79	4
"	$\text{HCOOH}$ , 100	-0.36	4
$\text{MeBr}$	$\text{EtOH}$ , 100	- .75	5
"	$\text{EtOH}$ , 50	+ .41	5,14
"	$\text{Me}_2\text{CO}$ , 50	+ .22	29
"	$\text{H}_2\text{O}$ , 100	+ .68	5
"	$\text{HCOOH}$ , 100 <sup>e</sup>	-1.78	5,16

(Table II continued)

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<u>Compound</u>	<u>Solvent</u>	<u>log (<math>k/k^0</math>)</u>	<u>Ref.</u>
EtBr	EtOH, 100	-0.77	5,17
"	EtOH, 50	+ .58	5,14
"	H <sub>2</sub> O, 100	+1.12	5
"	HCOOH, 100 <sup>f</sup>	-1.15	5,17
EtOTs	MeOH, 100	-0.28	5
"	EtOH, 100	- .57	5
"	EtOH, 50	+ .37	5
"	AcOH, 100	-2.38	5
n-BuBr	MeOH, 100 <sup>g</sup>	-0.36	7
"	MeOH, 96.7 <sup>g,h</sup>	- .21	7
"	MeOH, 69.5 <sup>g,h</sup>	+ .46	7
"	EtOH, 100	- .70	7
"	EtOH, 90 <sup>h</sup>	- .19	7
"	EtOH, 60 <sup>h</sup>	+ .27	7
"	HCOOH, 100 <sup>g</sup>	-1.14	18
$\phi$ CH <sub>2</sub> Cl	MeOH, 100	-0.26	5
"	EtOH, 100	- .85	5
"	EtOH, 50	+ .74	5
$\phi$ CH <sub>2</sub> OTs	MeOH, 100	- .29	5
"	EtOH, 100	- .78	5
"	AcOH, 100	-2.09	5
i-PrBr	EtOH, 100	-1.02	5
"	EtOH, 50	+0.86	5
"	H <sub>2</sub> O, 100	-1.99	5
"	HCOOH, 100	-0.14	5
i-PrOBs	MeOH, 100	- .37	8
"	EtOH, 100	- .81	8
"	AcOH, 100	-1.39	8
"	Ac <sub>2</sub> O, 97.5	-3.08	8

(Table II continued)

<u>Compound</u>	<u>Solvent</u>	<u>log (<math>k/k^\circ</math>)</u>	<u>Ref.</u>
PinOBs	MeOH, 100	-0.63	8
"	EtOH, 100	-1.29	8
"	AcOH, 100	-0.70	8
"	Ac <sub>2</sub> O, 97.5	-2.08	8
"	HCOOH <sup>i</sup>	+2.39	8
MeOCxOBs	MeOH, 100	-0.46	5
"	EtOH, 100	-1.02	5
"	EtOH, 50	+0.70	5
"	AcOH, 100	- .97	5,19
BrCxOBs	MeOH, 100	- .74	5
"	EtOH, 100	-1.42	5
"	EtOH, 50	+1.11	5
"	AcOH, 100	-1.12	5,19
$\phi$ CHClMe	MeOH, 100 <sup>j,k</sup>	-0.43	20
"	EtOH, 100 <sup>j,m</sup>	-1.50	20
"	Me <sub>2</sub> CO, 80 <sup>j,n</sup>	-1.12	20
"	AcOH, 100	-1.62	21
$\phi_2$ CHCl	MeOH, 96.7	-0.07	11
"	EtOH, 100	-1.51	22
"	EtOH, 90	-0.55	10
"	Me <sub>2</sub> CO, 90	-2.57	23
"	Me <sub>2</sub> CO, 80	-1.38	23
"	Me <sub>2</sub> CO, 70	-0.73	23
"	Me <sub>2</sub> CO, 50	+0.98	15
"	AcOH, 100 <sup>p</sup>	-2.36	11
"	HCOOH, 83.3	+2.61	11



(Table II continued)

<u>Compound</u>	<u>Solvent</u>	<u>log (k/k°)</u>	<u>Ref.</u>
$\phi_2\text{CHF}$	EtOH, 50	+1.61	11
"	AcOH, 100 <sup>P</sup>	+2.11	11
"	HCOOH, 83.3	+5.90	11
<u>t-BuCl</u>	MeOH, 100	-1.05	24
"	MeOH, 96.7	-0.72	24
"	MeOH, 69.5	+1.02	24
"	EtOH, 100	-1.98	12
"	EtOH, 90	-0.73	12
"	EtOH, 60	+1.14	12
"	EtOH, 50	+1.60	12
"	EtOH, 40	+2.15	12
"	Me <sub>2</sub> CO, 80	-0.68	12
"	Me <sub>2</sub> CO, 50	+1.29	25
"	H <sub>2</sub> O, 100	+3.55	8,26
"	AcOH, 100	-1.64	8
"	Ac <sub>2</sub> O, 97.5	-3.29	8
"	HCOOH, 83.3	+1.50	11
"	HCOOH, 100	+2.08	18
$\phi_3\text{CSCN}$	MeOH, 96.7	- .30	11
"	MeOH, 69.5	+ .40	11
"	EtOH, 40	+ .56	11
"	Me <sub>2</sub> CO, 80	- .28	11
"	Me <sub>2</sub> CO, 70	- .05	11
"	Me <sub>2</sub> CO, 50	+ .26	11

(Table II continued)

<u>Compound</u>	<u>Solvent</u>	<u>log (k/k°)</u>	<u>Ref.</u>
$\phi_3\text{COAc}$	MeOH, 96.7	+0.03	11
"	MeOH, 69.5	+ .90	11
"	EtOH, 60	+ .56	11
"	Me <sub>2</sub> CO, 80	-1.56	11
"	Me <sub>2</sub> CO, 50	+0.14	11
$\phi_3\text{CO}\phi\text{NO}_2$	MeOH, 69.5	+ .83	11
"	EtOH, 40	+1.25	11
"	Me <sub>2</sub> CO, 50	+0.37	11
"	AcOH, 100 <sup>P</sup>	+ .97	11
$\phi_3\text{CF}$	MeOH, 96.7	+ .11	11
"	MeOH, 69.5	+1.50	11
"	EtOH, 100	-1.73	11
"	EtOH, 40	+2.02	11
"	Me <sub>2</sub> CO, 70	-1.21	11
"	Me <sub>2</sub> CO, 50	+0.58	11
"	AcOH, 100 <sup>P</sup>	+1.76	11

(Footnote to Table II)

<sup>a</sup>These are decimal logarithms. For all compounds,  $\log k/k^\circ = 0.000$  in 80% ethanol by definition. For each compound, the temperature is that given in Table I.

<sup>b</sup>Symbols for compounds are explained in footnote a of Table I.

<sup>c</sup>Number after solvent is % by volume based on volumes before mixing; the residue is water except for 97.5%  $\text{Ac}_2\text{O}$  which is 2.5%  $\text{AcOH}$ ; Me, Et, Ac =  $\text{CH}_3$ ,  $\text{C}_2\text{H}_5$ ,  $\text{CH}_3\text{CO}$ .

<sup>d</sup>Calculated from data at 80° and 100°.

<sup>e</sup>Extrapolated from a higher temperature using  $\Delta E = 20.2 \text{ kcal.}$ <sup>27</sup>

<sup>f</sup>Extrapolated from a higher temperature using  $\Delta E = 19.8 \text{ kcal.}$ <sup>27</sup>

<sup>g</sup>Extrapolated from a higher temperature using  $\Delta E = 22.0 \text{ kcal.}$ <sup>11</sup>

<sup>h</sup>Interpolated from a plot of  $\log k$  vs. mole fraction of water.

<sup>i</sup>Extrapolated from a lower temperature using  $\Delta E = 27.1 \text{ kcal.}$ <sup>28</sup>

<sup>j</sup>Unfortunately the values used in these calculations were not the correct ones recorded here but were -1.37, -2.45 and -2.06 for methanol, ethanol, and 80% acetone respectively, which correspond to incorrectly calculated values tabulated by others<sup>8</sup> in the literature. We discovered this error subsequent to completion of the calculation.

<sup>k</sup>Extrapolated from a higher temperature using  $E = 21.7 \text{ kcal.}$ <sup>27</sup>

<sup>m</sup>Extrapolated from a higher temperature using  $E = 21.9 \text{ kcal.}$ <sup>27</sup>

<sup>n</sup>Extrapolated from a higher temperature using  $E = 21.8 \text{ kcal.}$ <sup>27</sup>

<sup>p</sup>The datum given was obtained in 99.3%  $\text{AcOH}$  - 0.7%  $\text{Ac}_2\text{O}$ , but is used for 100%  $\text{AcOH}$  since this compound is relatively little affected by traces of  $\text{H}_2\text{O}$  or  $\text{Ac}_2\text{O}$ .

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The data represent a wide range of structural variation. The compounds range from *p*-nitrobenzoyl and methyl to triphenylmethyl and from fluorides to arylsulfonates. Some have strong neighboring group participation and the pinacolyl compound even rearranges. The solvents range from anhydrous alcohols and water to glacial acetic acid and anhydrous formic acid.

Wishing to weight all the  $\log (k/k^0)$  values equally, we chose the condition

$$\sum_{146 \text{ data}} [\log (k/k^0)_{\text{obs.}} - (c_1 d_1 + c_2 d_2)] = \text{minimum}$$

to define the best fit. Thus no compound is given more weight than any other. Setting the partial derivative with respect to each other of the 25  $c_1$ , 25  $c_2$ , 17  $d_1$  and 17  $d_2$  unknown parameters equal to zero gave 84 simultaneous equations. These were solved by an iterative procedure (see method of calculation below) on the Mark IV digital computer of the Harvard Computation Laboratory.

The solution obtained was not unique. To make it unique it was necessary subsequently to impose four conditions (in addition to  $d_1 = d_2 = 0.00$  for 80% ethanol). These are in the nature of scale factors or normalization conditions for the calculated parameters and were chosen arbitrarily as follows.

$$c_1 = 3.00 \ c_2 \text{ for MeBr}$$

$$c_1 = c_2 = 1.00 \text{ for } t\text{-BuCl}$$

$$3.00 \ c_1 = c_2 \text{ for } \phi_3\text{CF.}$$

A renormalization to any other arbitrary assignment (any  $\alpha$  or  $\beta$ ) may be made easily using the equations

$$c_1^* = \alpha c_1 + (1 - \alpha) c_2$$

$$c_2^* = \beta c_1 + (1 - \beta) c_2$$

$$d_1^* = \left( \frac{1 - \beta}{\alpha - \beta} \right) d_1 + \left( \frac{-\beta}{\alpha - \beta} \right) d_2$$

$$d_2^* = \left( \frac{\alpha - 1}{\alpha - \beta} \right) d_1 + \left( \frac{\alpha}{\alpha - \beta} \right) d_2$$

$$d_1^* + d_2^* = d_1 + d_2$$

for new values (denoted by superscript stars).

Table III lists the values of the constants obtained. The values in parentheses are the ones arbitrarily assigned. Values based on very limited data are indicated by superscript letters referring to explanatory notes.

The ratio  $c_1/c_2$  is a convenient single number to characterize the reactivity of a compound. Compounds which discriminate relatively more highly among electrophilic reagents than among nucleophilic reagents tend to have low values for this ratio. As expected, this ratio decreases from *p*-nitro to *p*-methyl and in the order methyl, ethyl, *i*-propyl, *t*-butyl, benzhydryl, trityl.

The difference  $d_1 - d_2$  is a convenient single number to characterize the reactivity of a solvent. The most electrophilic solvents have the lowest values for this difference, with the difference decreasing in the order anhydrous alcohols, acetone-water and alcohol-water mixtures, water, glacial acetic acid, anhydrous formic acid.

Fig. 1 shows the correlation for several typical compounds using these compound and solvent constants.

Table III

VALUES OF COMPOUND AND SOLVENT CONSTANTS

Compound	$\epsilon_1$	$\epsilon_2$	$\epsilon_1/\epsilon_2$	Compound	$\epsilon_1$	$\epsilon_2$	$\epsilon_1/\epsilon_2$
$\text{NO}_2/\text{COCl}$	1.09	0.21	5.2	$i\text{-PrOBs}$	0.63	0.48	1.33
$\text{NO}_2/\text{COF}$	1.67	.49	3.4	$\text{MeOCxOBs}$	.57	.57	1.00
$\phi\text{COCl}$	0.81	.52	1.6	$\text{BrCxOBs}$	.80	.87	0.92
$\phi\text{COF}$	1.36	.66	2.1	$\text{PinOBs}$	.76	.87	0.86
$\text{Me}\phi\text{OOC1}$	0.82	.65	1.3	$\phi\text{CHClMe}$	1.47	1.75	.84
$\text{Me}\phi\text{COF}$	1.29	.80	1.6	$\phi_2\text{CHCl}$	1.24	1.25	.99
$\text{MeBr}$	0.80	.27	(3.0)	$\phi_2\text{CHF}$	0.32 <sup>a</sup>	1.17 <sup>a</sup>	.27 <sup>a</sup>
$\text{EtBr}$	.80	.36	2.2	$t\text{-BuCl}$	(1.00)	(1.00)	(1.00)
$\text{EtOTs}$	.65	.24	2.7	$\phi_3\text{CSCN}$	0.19	0.28	0.69
$i\text{-BuBr}$	.77	.34	2.2	$\phi_3\text{COAc}$	2.19 <sup>b</sup>	.77 <sup>b</sup>	—
$\phi\text{CH}_2\text{Cl}$	.74 <sup>a</sup>	.44 <sup>a</sup>	1.7 <sup>a</sup>	$\phi_3\text{CO}\phi\text{NO}_2$	0.18	.59	.31
$\phi\text{CH}_2\text{OTs}$	.69 <sup>a</sup>	.39 <sup>a</sup>	1.8 <sup>a</sup>	$\phi_3\text{OF}$	.37	1.12	(.33)
$i\text{-PrBr}$	.90	.58	1.5				
Solvent	$d_1$	$d_2$	$d_1-d_2$	Solvent	$d_1$	$d_2$	$d_1-d_2$
$\text{MeOH}, 100$	-0.05	-0.73	+0.68	$\text{Me}_2\text{CO}, 90$	-0.53 <sup>c</sup>	-1.52 <sup>c</sup>	+ 1.0 <sup>c</sup>
$\text{MeOH}, 96.7$	- .11	- .05	- .06	$\text{Me}_2\text{CO}, 80$	- .45	-0.68	+ 0.2
$\text{MeOH}, 69.5$	- .06	+1.32	-1.38	$\text{Me}_2\text{CO}, 70$	- .09 <sup>e</sup>	- .75 <sup>e</sup>	+ .7 <sup>e</sup>
$\text{EtOH}, 100$	- .53	-1.03	+0.49	$\text{Me}_2\text{CO}, 50$	- .25	+ .97	- 1.2
$\text{EtOH}, 90$	- .01 <sup>c</sup>	- .54 <sup>c</sup>	+ .52 <sup>c</sup>	$\text{H}_2\text{O}, 100$	-.44 <sup>d</sup>	+4.01 <sup>d</sup>	- 4.5 <sup>d</sup>
$\text{EtOH}, 80$	(.00)	(.00)	(.00)	$\text{AcOH}, 100$	-4.82	+3.12	- 7.9
$\text{EtOH}, 60$	- .22 <sup>d</sup>	+1.34 <sup>d</sup>	-1.56 <sup>d</sup>	$\text{Ac}_2\text{O}, 97.5$	-8.77 <sup>c</sup>	+5.34 <sup>c</sup>	-14.1 <sup>c</sup>
$\text{EtOH}, 50$	+ .12	+1.33	-1.21	$\text{HCOOH}, 83.3$	-4.44 <sup>c</sup>	+6.26 <sup>c</sup>	-10.7 <sup>c</sup>
$\text{EtOH}, 40$	- .26	+2.13	-2.38	$\text{HCOOH}, 100$	-4.40	+6.53	-10.9

(Footnotes to Table III)

<sup>a</sup> Somewhat doubtful because based on only three  $\log (k/k^0)$  values.

<sup>b</sup> Especially badly fixed by the data because based on only five  $\log (k/k^0)$  values for very similar media: none was an absolute alcohol or contained over 50% water or any acetic acid or formic acid.

<sup>c</sup> Use with caution. Not well fixed by the data because based on only three compounds.

<sup>d</sup> Based on only four compounds.

<sup>e</sup> Based on aromatic compounds only, hence may give poor predictions for aliphatic compounds.



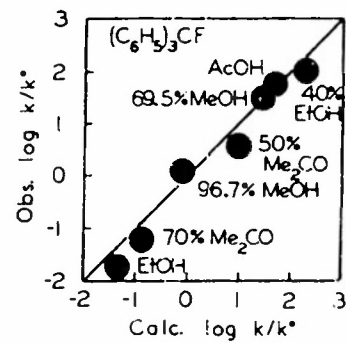
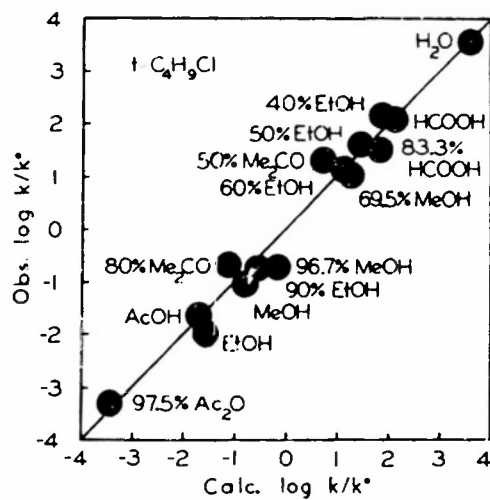
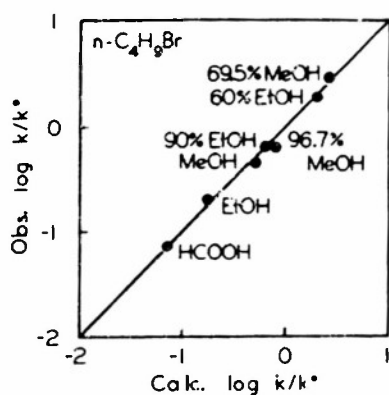
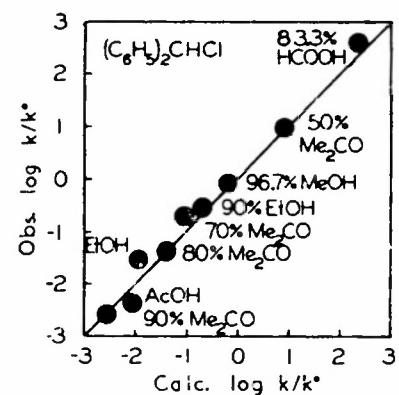
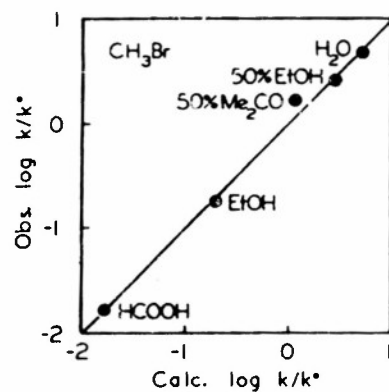
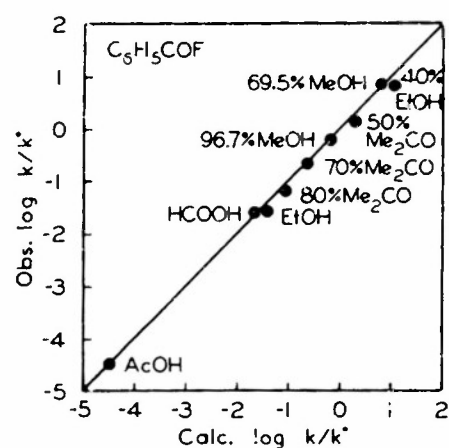
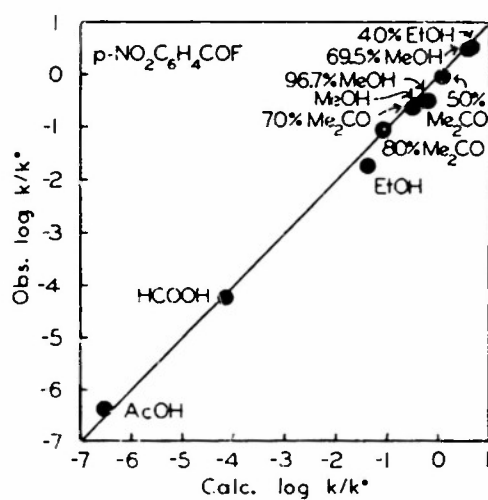
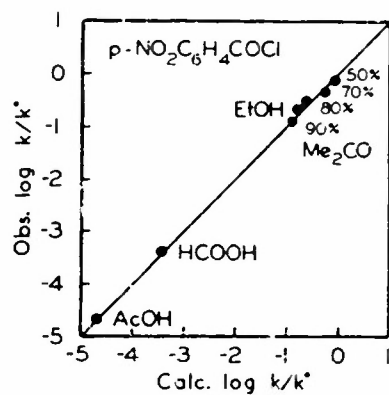


Table IV lists some measures of fit.<sup>2</sup> The compound with the largest  $\epsilon$  (mean error in  $\log k_{\text{calc.}}$ ) is *t*-butyl chloride and for it our measure of fit,<sup>2</sup>  $\Phi$ , is typical and excellent, viz. 85%. Figs. 1 - 8 show typical plots of the fits obtained. The largest individual error is for benzoyl chloride in methanol and corresponds to a factor of 4.4 in  $k$ . The mean  $\epsilon$  for all compounds is 0.124 (factor of 1.33 error in  $k$ ). For typical solvents  $\epsilon$  is 0.12 for methanol ( $n = 12$ ), 0.22 for 50% acetone ( $n = 13$ ), 0.07 for acetic acid ( $n = 18$ ), and 0.04 for formic acid ( $n = 10$ ). The fit is about as good for the extreme compounds and solvents studied as for the ones of intermediate reactivity.

Table IV  
MEASURES OF FIT<sup>2</sup> FOR CERTAIN COMPOUNDS

Compound	$n$	$\epsilon$	$\Phi, \%$
$\text{NO}_2\phi\text{COCl}$	7	0.07	95
$\text{NO}_2\phi\text{COF}$	10	.15	90
$\phi\text{COCl}$	12	.23	72
$\phi\text{COF}$	9	.11	91
MeBr	5	.06	93
<i>n</i> -BuBr	7	.05	89
$\phi\text{CHCl}$	9	.19	84
<i>t</i> -BuCl	15	.25	85
$\phi_3\text{CF}$	7	.25	79

Discussion.- The results were compared with those using other equations in paper XI.<sup>2</sup> The correlation is particularly gratifying for p-nitrobenzoyl chloride and triphenylmethyl fluoride, which gave almost random scatter plots<sup>11</sup> of  $\log (\underline{k}/\underline{k}^0)_{\text{obs.}}$  vs.  $\log (\underline{k}/\underline{k}^0)_{\text{calc.}}$  when the equation<sup>using</sup>

$$\log (\underline{k}/\underline{k}^0) = \underline{mY}$$

Howard H.

Acknowledgment.- We are greatly indebted to Professor Aiken and the Air Force for making the Harvard Mark IV digital computer available, and especially to Mr. Peter F. Strong and Mr. J. Orten Gadd, Jr. of the Harvard Computation Laboratory for setting up and solving this mathematical problem on the computer. Their abbreviated description of the procedure is given below.

#### METHOD OF CALCULATION

In this problem it is required to find the best values of  $\underline{a}_1, \underline{b}_1, \underline{c}_j, \underline{d}_j$  to represent a given matrix of the form  $\underline{E}_{ij} \underline{Z}_{ij}$  by the scalar product

$$\underline{Z}_{ij} = \underline{a}_1 \underline{c}_j + \underline{b}_1 \underline{d}_j, \quad i = 1, 2, \dots, \underline{m}$$

$$j = 1, 2, \dots, \underline{n}.$$

Not all possible elements  $\underline{Z}_{ij}$  are given; the elements  $\underline{E}_{ij}$  are introduced to form an existence matrix such that  $\underline{E}_{ij} = 1$  if the corresponding  $\underline{Z}_{ij}$  is given and  $\underline{E}_{ij} = 0$  otherwise.

To obtain a least squares fit, it is required that the quantity

$$\epsilon^2 = \sum_i \sum_j \underline{E}_{ij} (\underline{Z}_{ij} - \underline{a}_1 \underline{c}_j - \underline{b}_1 \underline{d}_j)^2$$

be minimum. From this it follows that

$$\frac{\partial}{\partial \underline{a}_1} (\epsilon^2) = \frac{\partial}{\partial \underline{b}_1} (\epsilon^2) = \frac{\partial}{\partial \underline{c}_j} (\epsilon^2) = \frac{\partial}{\partial \underline{d}_j} (\epsilon^2) = 0$$

for all  $i$  and  $j$ . Carrying out the differentiations one obtains a system of  $2 (\underline{m} + \underline{n})$  non-linear simultaneous equations as follows:

$$a_1 \sum_j E_{1j} c_j^2 + b_1 \sum_j E_{1j} c_j d_j = \sum_j E_{1j} c_j z_{1j} \quad (1)$$

$$a_1 \sum_j E_{1j} c_j d_j + b_1 \sum_j E_{1j} d_j^2 = \sum_j E_{1j} d_j z_{1j} \quad (2)$$

$$c_j \sum_i E_{ij} a_i^2 + d_j \sum_i E_{ij} a_i b_i = \sum_i E_{ij} a_i z_{ij} \quad (3)$$

$$c_j \sum_i E_{ij} a_i b_i + d_j \sum_i E_{ij} b_i^2 = \sum_i E_{ij} b_i z_{ij} \quad (4)$$

If approximations to the values of  $c_j$  and  $d_j$  be given, Equations (1) and (2) can be solved simultaneously to give approximate values of  $a_1$  and  $b_1$ . Then Equations (3) and (4) can be solved to give new approximations to the values of  $c_j$  and  $d_j$ . This is a simple process since, for a given value of  $i$ , Equations (1) and (2) are just a pair of linear simultaneous equations involving  $a_1$  and  $b_1$  as unknowns, and a similar remark applies to Equations (3) and (4).

Although Equations (1), (2), (3) and (4) may be used as an iterative process to obtain a solution of the problem it was decided to employ an extrapolation process<sup>30</sup> in order to decrease the time required

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(30) The principle on which this process is based was suggested by Dr. R. E. Clapp.

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to obtain the answer. Let the sets of numbers  $a_1$ ,  $b_1$ ,  $c_j$  and  $d_j$  obtained after the  $n$ -th iteration form the vector  $V_n$ . Let

$$V_{n+1} - V_n = D_n.$$

Now  $\epsilon^2$  may be written as

$$\epsilon^2 = f(V_{n+1})$$

since  $\epsilon^2$  is a function of the variables which form the components of  $V_n$ .

One may calculate

$$f_0 = f(V_{n+1})$$

$$f_1 = f(V_{n+1} + hD_n)$$

$$f_2 = f(V_{n+1} + 2hD_n)$$

where  $h$  is a scalar. Now assume that  $f(V_{n+1} + xD_n)$  is approximately a quadratic in  $x$  (in practice the validity of this assumption depends mainly on the choice of  $h$ ).

Then

$$f(V_{n+1} + xD_n) \approx f_0 + u\Delta f + \frac{u(u-1)}{2} \Delta^2 f$$

where

$$u = \frac{x}{h}, \quad \Delta f = f_1 - f_0, \quad \Delta^2 f = f_2 - 2f_1 + f_0.$$

This expression of  $f$  may now be minimized with respect to  $x$  by setting the derivative equal to zero.

One finds that  $f(V_{n+1} + sD_n)$  is minimum for

$$s = h \left( \frac{1}{2} - \frac{\Delta f}{\Delta^2 f} \right),$$

and the vector  $V = V_{n+1} + sD_n$  may be used to start a new series of iterations. In the course of the problem values of  $s$  of 10-20 were usual, although much larger numbers were encountered in certain circumstances. The size of  $s$  is, of course, dependent to some extent on the number of iterations between extrapolations. This number was varied somewhat in the course of running the problem, though it was usually found that three to five iterations gave good results. Running time for this problem, starting either with given approximations or with all starting values equal to unity, was about one hour.